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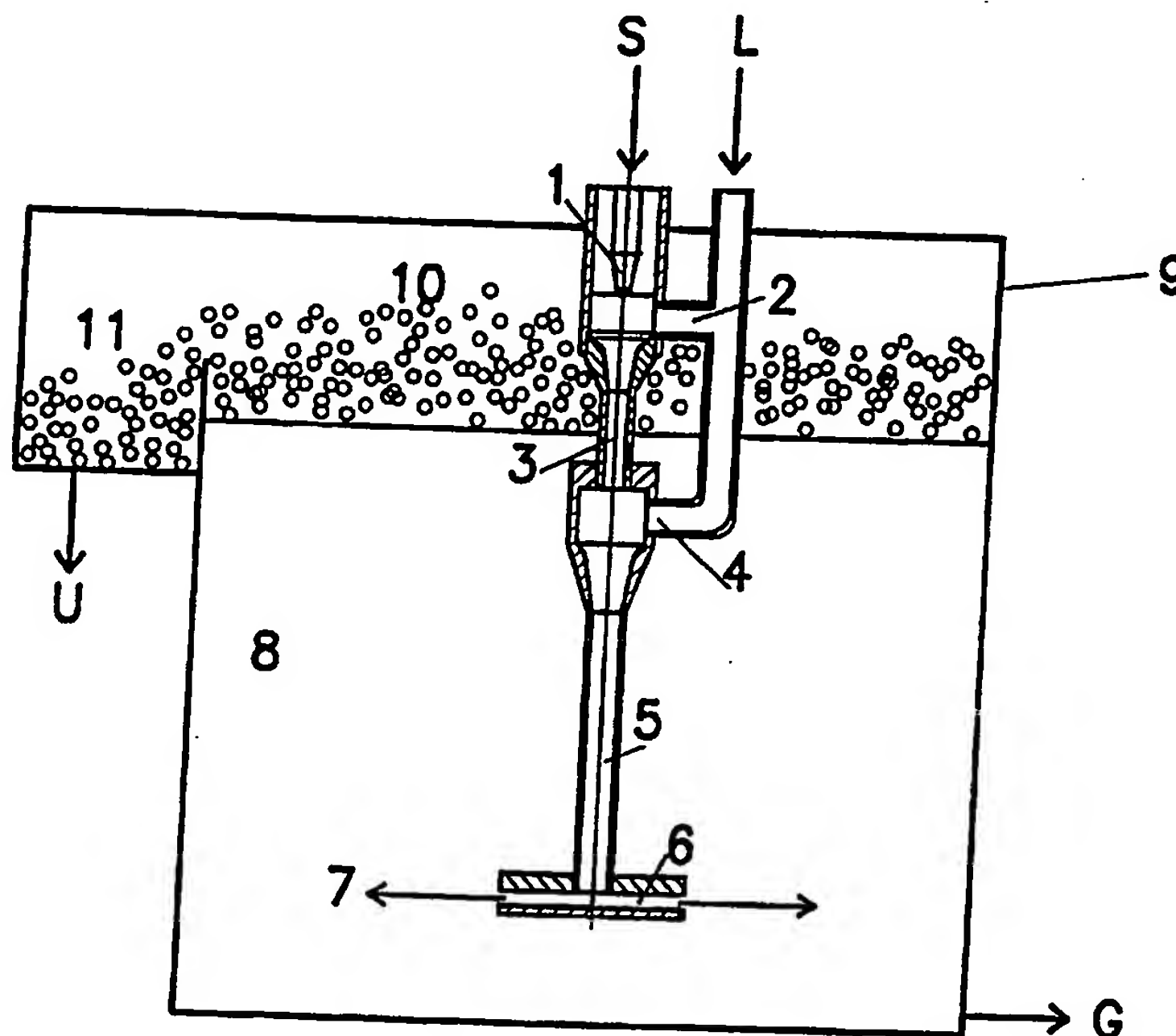
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(54) Title: PROCESS AND DEVICE FOR AERATING DISPERSIONS



(57) Abrégé/Abstract:

The invention refers to a process for aerating dispersions, particularly for flotation of pulp suspensions in the deinking process, where the pulp suspension containing dirt particles is sprayed into a tank together with gas, particularly air. It is mainly characterised by the gas, particularly air, being sucked in by the effect of the injector at a minimum of two successive points 2, 4, 12 and mixed with the suspension. The invention also refers to a device for implementing the process.

ABSTRACT

The invention refers to a process for aerating dispersions, particularly for flotation of pulp suspensions in the deinking process, where the pulp
5 suspension containing dirt particles is sprayed into a tank together with gas, particularly air. It is mainly characterised by the gas, particularly air, being sucked in by the effect of the injector at a minimum of two successive points 2, 4, 12 and mixed with the suspension. The invention also refers to a device for implementing the process.

Process and Device for Aerating Dispersions

The invention relates to a process for aerating dispersions, particularly for flotation of pulp suspensions in the deinking process, where the pulp suspension containing dirt particles is sprayed into a tank together with gas, particularly air. In addition, the invention relates to a device for
5 implementing the process.

Deinking flotation is a mechanical process for removing impurities and ink particles from pulp suspensions produced particularly in waste paper treatment. This process requires the generating of gas bubbles in the appropriate quantity and size distribution. Hydrophobic substances or
10 substances to which ampholytics are added to make them hydrophobic, such as ink particles or stickies, are carried to the surface of the liquid by the gas bubbles adhering to them and can be removed from the surface as scum. This is referred to as selective flotation because the pulp is discharged with the accept due to its hydrophile nature. Processes of this
15 type are known in numerous geometric modifications, for example from DE 41 16 916 C2 or EP 0 211 834 B1, and have reached a high technical standard. Further, it has also proved successful to use self-priming injectors to generate gas bubbles and mix these with the pulp suspension. These injectors basically comprise a propulsive jet nozzle, a mixing or
20 impulse exchange pipe, and a diffuser. Here, the liquid flow emerging from the propulsive jet nozzle according to the open jet principle generates underpressure. As a result, gas is sucked in and mixed with the liquid as a result of the impulse exchange between liquid and gas in the mixing pipe. At the exit from the diffuser used for energy recovery a dispersion of
25 pulp and bubbles is formed. Use of the known processes and injectors, however, has shown several disadvantages in selective flotation of pulp suspensions.

The suction effect of the known injectors in operation with pulp suspensions is too weak and the bubble size distribution generated by the injector known does not have the optimum design to meet the requirements of selective flotation.

- 5 The invention is, therefore, based on the task of designing an injector with greater suction effect and optimum bubble size distribution for use in deinking flotation.

The process according to the invention is thus characterised by the gas, particularly air, being sucked in by the effect of the injector at a minimum
10 of two successive points and mixed with the suspension. Due to suction taking place in stages, the pulp can be loosened by the gas in the first stage, thus achieving a better spread of the free jet in the second stage, resulting in improved suction effect and corresponding bubble generating, particularly with a reduction in the fine bubble portion to avoid solids
15 losses.

An advantageous further development of the invention is characterised by some 20 to 95% of the entire quantity of gas, particularly air, sucked in being taken in the first stage. Since intake of the quantity of gas, particularly air, is divided over several suction points, more even mixing of
20 the suspension with the gas is obtained. This allows a specific suitable bubble size to be set.

A favourable configuration of the invention is characterised by the gas and liquid flow obtained by suction and mixing being transferred in a free jet after the first stage. As a result, use of the kinetic energy of the jet, in
25 particular, can be improved for renewed intake of gas.

A favourable further development of the invention is characterised by the gas or air loading of the pulp suspension directly after being sprayed in amounting to approximately 50 – 150%.

The invention also refers to a device for aerating dispersions, particularly a flotation device for deinking pulp suspensions with an injector, characterised by at least two suction points being arranged in series in flow direction. Due to suction taking place in stages, the pulp can be loosened by the gas in the first stage, thus achieving a better spread of the free jet in the second stage, resulting in improved suction effect and corresponding bubble generating, particularly with a reduction in the fine bubble portion to avoid solids losses.

A favourable further development of the invention is characterised by the injection channel widening after the first suction point. Thus, the kinetic energy of the jet can be put to good use in a favourable manner.

An advantageous further development of the invention is characterised by a panel being mounted at the end of the injector channel across the flow direction. This panel acts as a radial diffuser to recover energy from the liquid jet.

An advantageous configuration of the invention is characterised by the panel being mounted on a slant to the flow direction.

A favourable further development of the invention is characterised by the panel containing internals for targeted guidance of the flow. As a result, the injector can also be mounted in any desired position in the flotation cell.

A favourable configuration of the invention is characterised by a minimum of two injectors being mounted in parallel in the form of an injector group. With this design it is also possible to handle large throughputs accordingly.

In the following the invention is described in examples and with reference to the drawings, where Fig. 1 shows an arrangement of a variant of the invention in a flotation cell, Fig. 2 an alternative variant, Fig. 3 a further

variant of the invention, Fig. 4 a variant with three gas intake points, Fig. 5 a variant with injector group, Fig. 6 a diagram of a bubble diameter distribution pattern, Fig. 7 the air loading for a conventional injector compared with a device according to the invention, and Fig. 8 the flotation loss of a device according to the invention compared with a state-of the art device.

Figure 1 shows a diagram of the flotation unit in which the device according to the invention is installed. The flotation cell 9 is largely filled with suspension 8, on the surface of which scum 10 forms, which contains as large a portion as possible of impurities and ink particles to be removed by flotation. This scum flows through a conduit 11 as overflow U. The pulp suspension S enters the injector through the propulsive jet nozzle 1. Due to the open jet principle air is added at the first suction point 2 and mixed into the pulp suspension in the first impulse exchange pipe 3. The pulp suspension loosened in this way by the air bubbles sucks in more air 4 at the second suction point and this air is mixed into the suspension in the second impulse exchange pipe 5. The air suction points are connected in this case to a pipe protruding out of the suspension and into which air L enters at the surface of the suspension. The dispersion 7 of bubbles and pulp leaves the injector after passing through a radial diffuser 6 for energy recovery purposes. The bubbles formed in this way adhere to the hydrophobic impurities and carry them to the surface. The suspension cleaned by flotation leaves the flotation cell as accept pulp G.

Figure 2 contains an alternative variant of an injector according to the invention, where the gas intake fittings, for example, are mounted on different sides. A significant difference to Fig. 1, however, is that a conically widening diffuser is installed after the second stage.

Figure 3 shows a device according to the invention with a conically shaped first impulse exchange pipe 3, where a second propulsive jet nozzle is

used analogous to the propulsive jet nozzle 1 so that high suction efficiency is also achieved in the second stage.

Figure 4 contains a design according to the invention in which three air intake points 2, 4, 12 are provided, with a diffuser shown after the third
5 impulse exchange pipe 13.

Figure 5 shows a variant as injector group, where two injectors are mounted here in parallel beside each other. This arrangement comprises a top section, in which the propulsive jet nozzles 1 are mounted, a common intermediate area into which the air intake fitting 2 leads, also a
10 block with impulse exchange pipes 3 operating in parallel. This block is connected in turn to a common intermediate area into which the gas intake pipe 4 leads. This is adjoined by a common block where the second impulse exchange pipes 5 are mounted. Finally, both impulse exchange pipes 5 lead into a radial diffuser 6. It would also be possible
15 basically to combine several injectors in an injector group of this kind.

Figure 6 now shows the bubble diameter distribution pattern of a conventional injector compared with that of an injector according to the invention. This shows that the injector according to the invention contains significantly fewer bubbles with a diameter < 0.5 mm than the state-of-the-
20 art injector. Here the reduction is approximately 50%. Unlike the conventional injector, however, the distribution spectrum is still retained. Overall there are fewer solids (fibre) losses as a result.

The suction effect of an injector is determined by the propulsive jet throughput, the diameter of the propulsive jet nozzles, the liquid cover and
25 the density of the propulsive jet. Suction characteristics of this type are illustrated in Figure 7. Here the air loading q_G/q_L is shown as a function of the Froude number. The illustration shows that, compared with conventional injectors, this air loading can be increased significantly with the device according to the invention.

Figure 8 contains a diagram of a flotation result at the same air intake compared with that of a conventional injector. The diagram shows that the overall fibre loss could be reduced by approximately one third. With the present invention, however, it is possible to inject much more air and
5 thus, also improve removal of impurities.

Patent Claims

1. Process for aerating dispersions, particularly for flotation of pulp suspensions in the deinking process, where the pulp suspension containing dirt particles is sprayed into a tank together with gas, particularly air, **characterised by** the gas, particularly air, being sucked in by the effect of the injector at a minimum of two successive points and mixed with the suspension.
2. Process according to Claim 1, **characterised by** some 20 to 95% of the entire quantity of gas, particularly air, sucked in being taken in the first stage.
3. Process according to Claim 1 or 2, **characterised by** the gas and liquid flow obtained by suction and mixing being transferred in a free jet after the first stage.
4. Process according to one of Claims 1 to 3, **characterised by** the gas or air loading of the pulp suspension directly after being sprayed in amounting to approximately 50 – 150%.
5. Device for aerating dispersions, particularly a flotation device for deinking pulp suspensions, with an injector, **characterised by** at least two suction points (2, 4, 12) being arranged in series in flow direction.
6. Device according to Claim 5, **characterised by** the injection channel widening after the first suction point (2).
7. Device according to Claim 5 or 6, **characterised by** a panel being mounted at the end of the injector channel across the flow direction and this panel acting as a radial difusor (6).

8. Device according to Claim 7, **characterised by** the panel being mounted on a slant to the flow direction.
9. Device according to Claim 7, **characterised by** the panel containing internals for targeted guidance of the flow.
- 5 10. Device according to one of Claims 5 to 9, **characterised by** a minimum of two injectors being mounted in parallel in the form of an injector group.

Fig.1

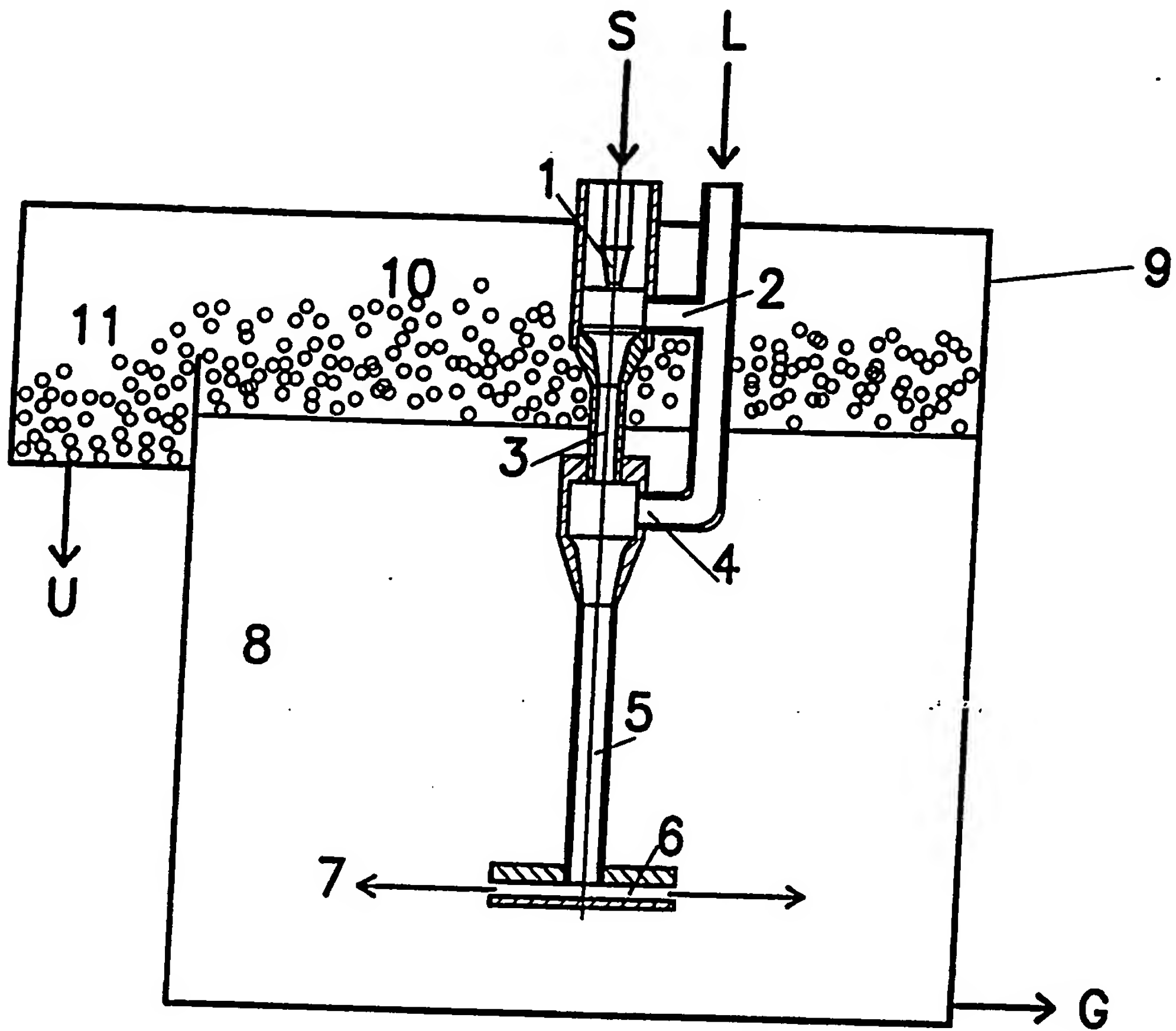


Fig.2

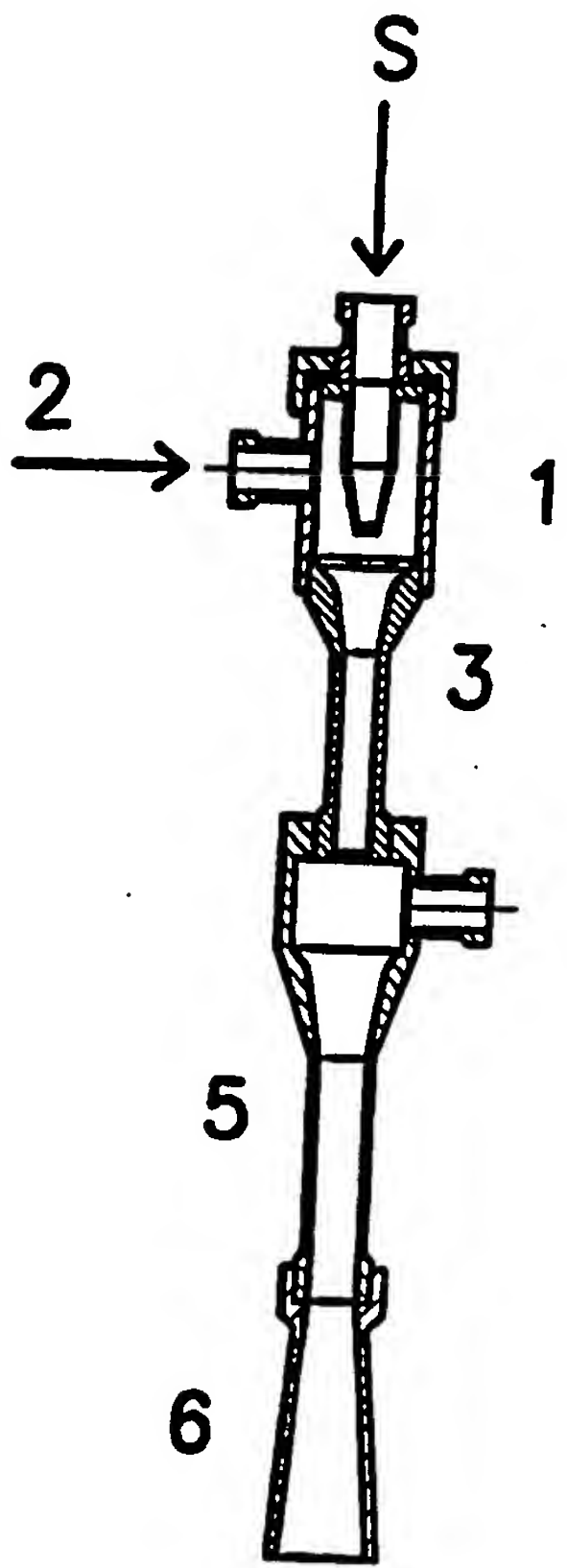


Fig.3

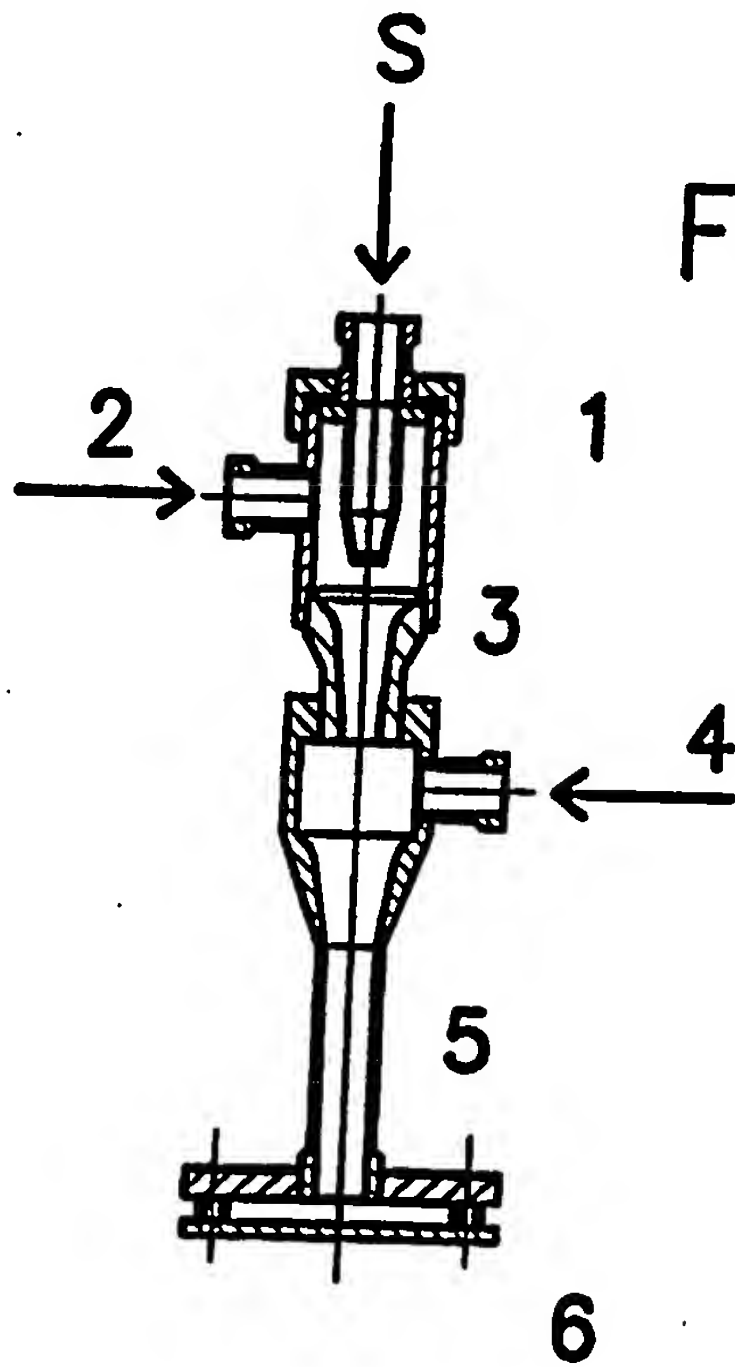


Fig.4

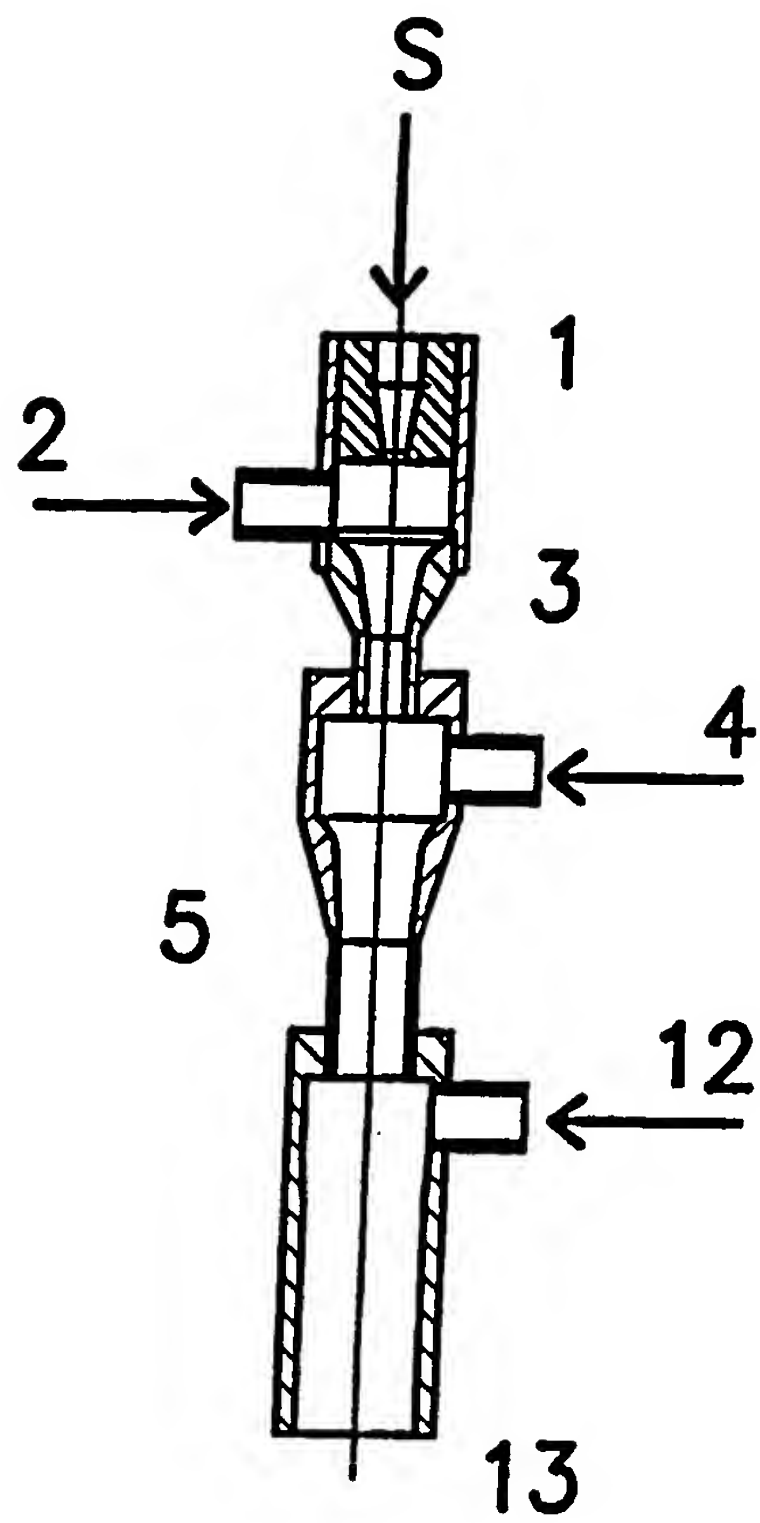
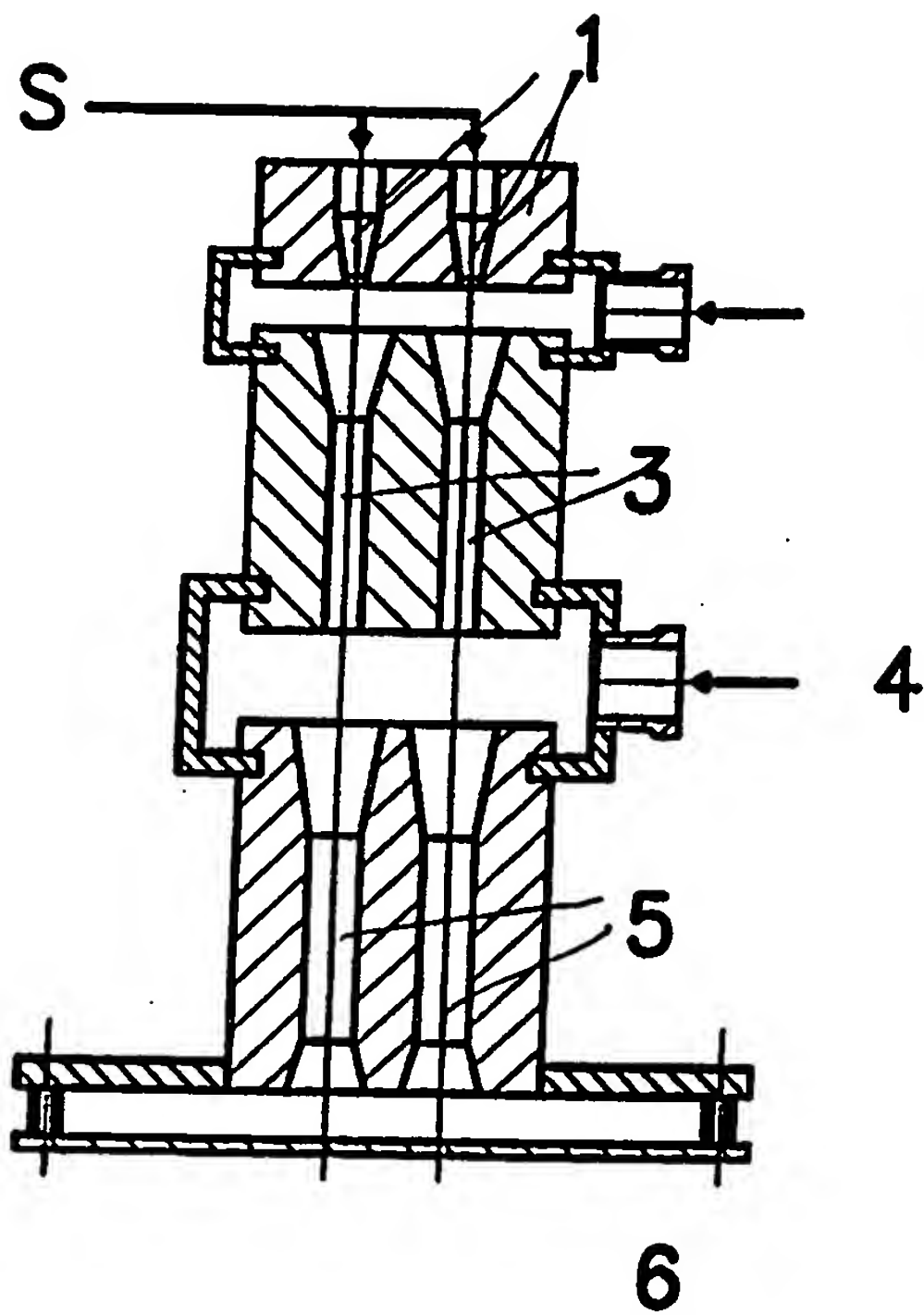


Fig.5



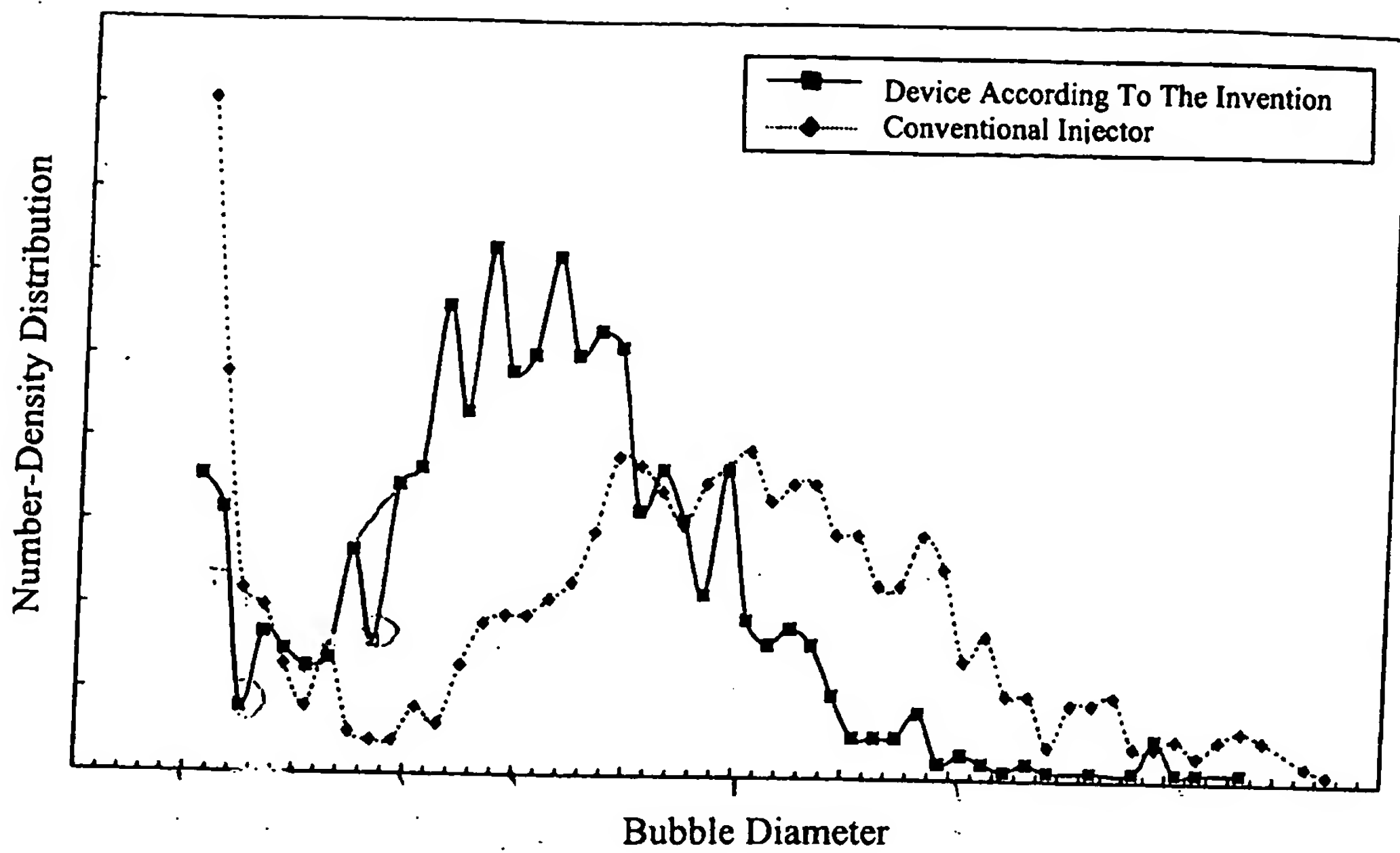


Fig. 6

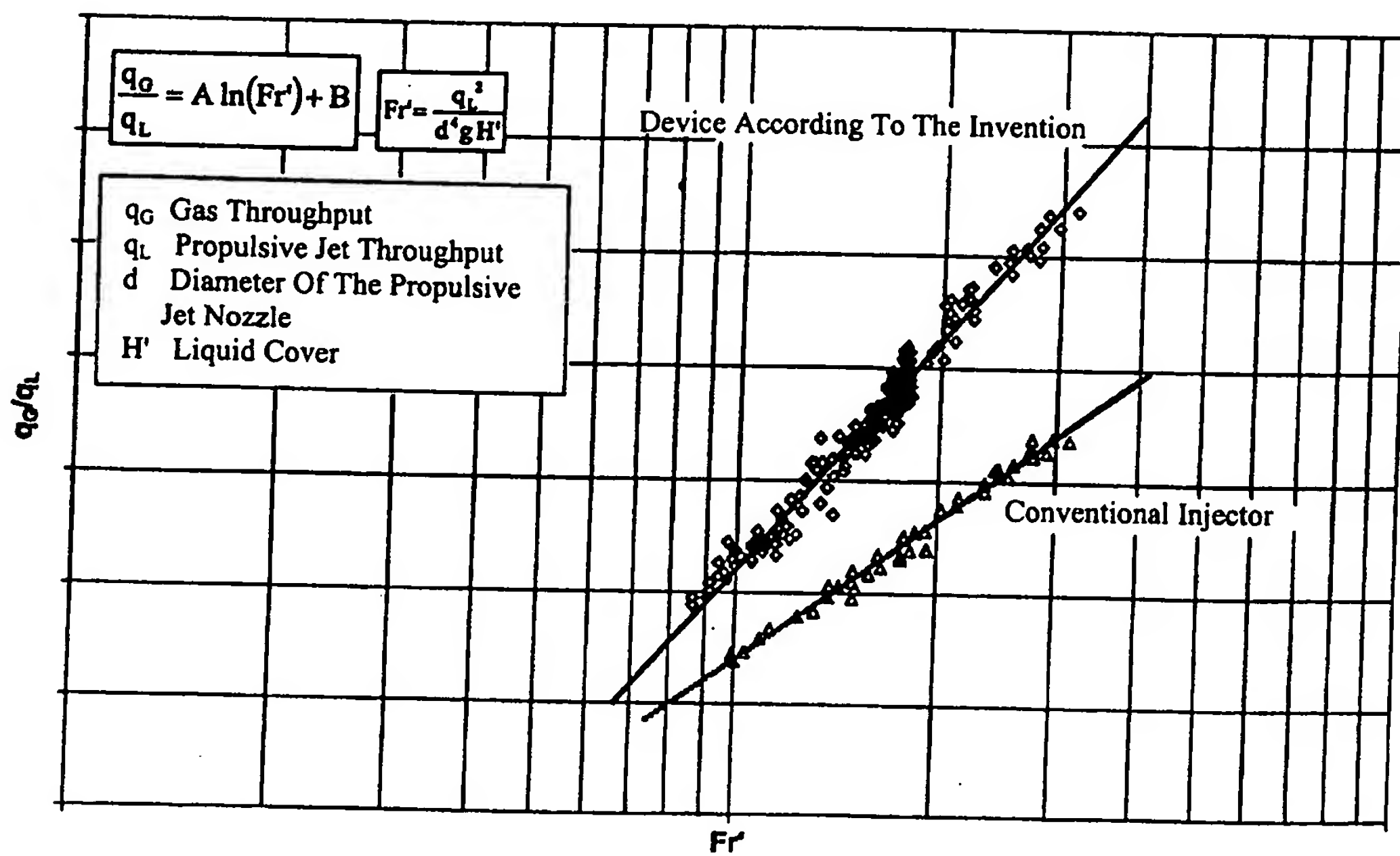


Fig. 7

Flotation Results
At The Same Air Intake

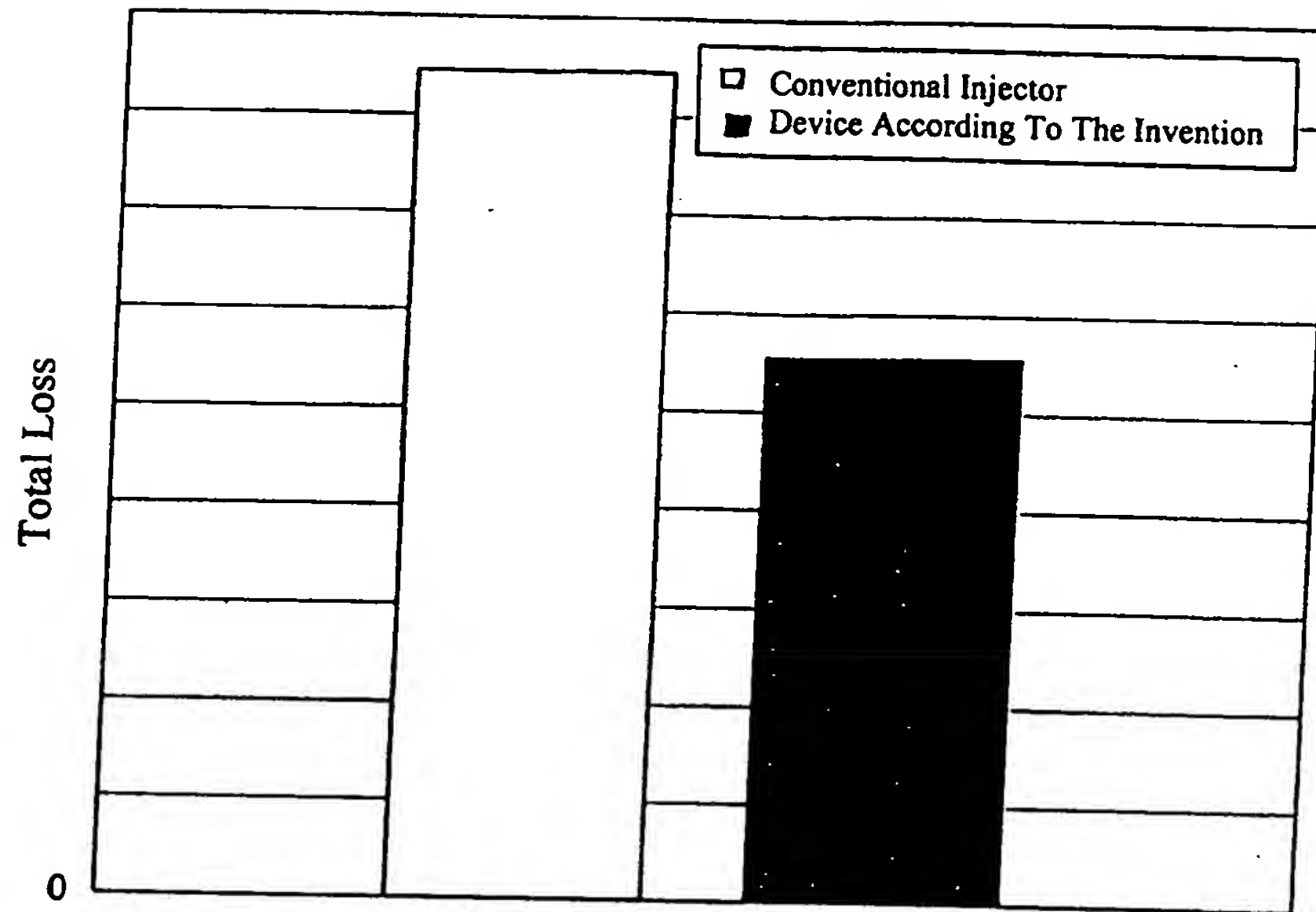


Fig. 8